

(57) **Abstract:** A dry process for the cleaning of precision surfaces of semiconductor wafers by using process materials such as carbon dioxide and useful additives such as cosolvents and surfactants, where the process materials are applied exclusively in gaseous and supercritical states. Soak and agitation steps are applied to the wafer, including a rapid decompression of the process chamber (10) after a soak period at higher supercritical pressure, to mechanically weaken, break up the polymers and other materials sought to be removed, combined with a supercritical fluid flush to carry away the loose debris.

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For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

SUPERCRITICAL FLUID CLEANING PROCESS FOR PRECISION SURFACES

This application relates and claims priority for all purposes to pending U.S. applications s/n 60/205335 filed 18 May 2000, s/n 60/267916 filed 09 February 2001, s/n 5 60/197519 filed 18 April 2000, s/n 09/837507 filed 18 April 2001, s/n 09/632770 filed 04 August 2000, s/n 60/147251 filed 05 August 1999, s/n 60/155454 filed 20 September 1999, and s/n 09/665932 filed 20 September 2000.

Field of Invention:

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This invention relates to methods for cleaning precision surfaces of wafers with supercritical fluids; and in particular to methods of cleaning wafers using rapid decompression techniques at supercritical state combined with full flow washing action.

15 Background

Semiconductor device manufacturing or IC fabrication requires precisely controlled quantities of impurities to be introduced into tiny regions of the silicon substrate. Subsequently these regions must be interconnected to create components and 20 electronic circuits. Lithographic processes create the patterns that define such regions. That is, a layer of photoresist materials is first spin-coated onto the wafer substrate. Next, this resist is selectively exposed to radiation such as ultraviolet light, electrons, or x-rays. An exposure machine, called stepper, and mask, called reticle, are used to effect the desired selective exposure. The patterns in the resist are formed when the wafer 25 undergoes a subsequent development step. The areas of resist remaining after development protect the substrate regions, which they cover.

Locations from which resist has been removed can be subjected to a variety of subtractive (e.g. etching) or additive (e.g. ion implantation) processes that transfer the 30 pattern onto the substrate surface. An advance integrated circuit can have up to 30 or more masking layers. Approximately one-third of the total cost of semiconductor

manufacturing can be attributed to microlithographic processing; ref. Silicon Processing for the VLSI Era, S. Wolf and R.N. Tauber, Vol. 1, 2nd edition, Lattice Press, Sunset Beach, CA, 2000, pp. 488, incorporated herein by reference.

5 The above mentioned residues are required to built up in the manufacturing process. Sidewall polymers, also called veils or via veils are a beneficial by-product, or artifact of RIE providing means for anisotropic etch to produce high aspect ratio vias. Compositionally sidewall polymers are generally low molecular weight fluoropolymers, that form from a combination of ion bombardment of the photoresist mask and fluorine in
10 the etch gas chemistry. Upon back-sputtering from the via base metal ions are incorporated in the via veil, which tend to oxidize at high temperature (250°C to 400°C) oxygen plasma based photoresist stripping to become insoluble.

After etching (wet or dry) or ion implantation photoresist has to be removed.
15 There are different degrees of difficulty required to do this, depending on the prior process. High-temperature hard bakes, plasma etch residues, sidewall polymers in contact holes and electrical interconnect trenches, ion implantation crusting, shrinking feature sizes, and new polymeric types of insulating material including low-k materials, all present challenges for the resist removal process. Both wet and dry stripping methods are
20 being used. Plasma ashing as a dry method is currently the method of choice for the back-end of the fabrication process where the electrical interconnects are manufactured.

During plasma ashing, photoresist is removed by oxygen energized in a plasma field, which oxidizes the resist components to gases that are removed from the process
25 chamber by a vacuum pump. Microwave, RF and UV-ozone sources generate the plasma. The disadvantage of plasma resist stripping is its ineffectiveness in the removal of metal ions and residues after dry etching, or reactive ion etching (RIE), namely sidewall polymers in vias, contact holes and trenches; ref. Microchip Fabrication, P. van Zant, 3rd edition, McGraw Hill, New York, 1997, pp. 273, incorporated herein by reference.

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To complete the photoresist stripping process all residues have to be removed. This is typically done in wet chemical cleaning stations. After that the wafer has to be rinsed in deionized water and is finally dried. The process is called post-strip cleans.

5 The problems associated with the prior art methods of photoresist stripping by plasma ashing (PA) and residue removal can be summarized as follows:

- PA is performed at high temperatures of 250° - 400°C, adding to the thermal budget of the wafer;
- 10 □ after PA residues are left in vias and trenches that need additional wet chemical treatment;
- PA is not efficient for removing mobile metallic ion contamination;
- PA can cause radiation damage of the electronic circuits;
- PA of photoresist after ion implantation can lead to "resist popping" littering the
- 15 wafer with particulate matter;
- with PA, selectivity between photoresist and low-k materials is bad and low-k material may be mechanically affected;
- PA can modify the dielectric constant of low-k material due to charge damage;
- post-strip wet chemical treatment may modify the low-k material in its electrical
- 20 properties;
- shrinking dimensions of features below 0.18 μm present a problem for wet chemistry as post-strip cleans method, because of surface tension issues.

There are ongoing efforts to improve the efficiency of PA. A new process has

25 been reported recently where during ashing fluorine-based gases are added that render residues water soluble. In a subsequent rinse step with deionized water the residues are being removed; ref. Manufacturing Qualification of an All Dry DeVeil Process, Richard Bersin, et al., The 197th Meeting of the Electrochemical Society, Toronto, 2000,

30 incorporated herein by reference. Although the process is touted "all dry", a wet rinsing step has to follow and therefore problems with surface tension of water occur for small features as is typical for wet methods.

Alternative methods are being investigated. Some of them are still wet chemical based (Chilled Ozone - IMEC, Belgium; SO_3 + DI water rinse - Anon, USA) and therefore will have problems with processing small features. Laser stripping is a method developed in two modifications by different companies (Oramir, Israel; Radiance, USA). Both use laser energy to remove the photoresist. In one case environmentally critical process gases NF_3 or CF_4 are being added (Oramir), or inert gas is being used (Radiance). There is no indication as of today that these methods will find broad acceptance in the semiconductor industry. Other methods aim at the post-strip cleaning process with equipment either in the development phase or being used occasionally as post treatment tools (Dry Ice Spray - ATS Eco-Snow, USA; Charged Microclusters - Phrasor Scientific Inc., USA; Argon/Nitrogen Cryogenic Aerosol Cleaning - FSI International, USA).

Another technology being investigated for its obvious potential advantages is the use of supercritical fluids for wafer cleaning, particularly with carbon dioxide. This approach takes advantage of the supercritical state of a process chemical, which is another state of matter, also called phase, in addition to solid, liquid and gas. Sometimes the supercritical phase is referred to as "dense gas", "compressible liquid", or "supercritical fluid". Among the prior art on the subject, are ((I'll cite the LANL Patents)). There is considerable other art on the subject. However, there has been a dearth of understanding as to the best mode in which to apply the technology in a practical, easily automated process so as to produce the desired quality of cleaning, in the shortest amount of time, on a repetitive basis and at an affordable cost. It is this area of the art to which the following invention is directed.

In the description of the invention that follows, the supercritical phase of the process chemical is referred to as supercritical fluid. In this dense state the process substance fills the process chamber completely like a gas with the molecules interacting strongly. This leads to new properties of the process material that are crucial to the cleaning process. The supercritical state is characterized by a critical point, which constitutes of a critical pressure p_c and a critical temperature T_c . At the critical point the

density of the vapor and the liquid are identical. A material is in its supercritical state, if both, pressure and temperature are at or exceed the critical values.

Supercritical fluids have long been known for their abilities to dissolve organic contaminants. Their ability to display a wide range of solvent characteristics and the ability to tune solubility with small changes in temperature and pressure were identified early on. The gas-like diffusivity and low surface tension combined with liquid-like densities are important since these qualities enhance the cleaning effectiveness on parts, which have very small features (e.g. vias and trenches on semiconductor devices), or contain materials where selectivity of the supercritical fluid to one or the other component is a requirement, for example, between low-k material and photoresist in the fabrication of semiconductor devices; ref. Precision Cleaning With Supercritical fluid: A Case Study, John. E. Giles, et. al. in "Supercritical Fluid Cleaning - Fundamentals, Technology and Applications", John McHardy, Samuel P. Sawan, ed., Noyes Publications, Westwood, NJ, USA, 1998, pp. 198, incorporated herein by reference

The effectiveness of supercritical fluids for cleaning can be improved. The use of binary and multi-component fluids is driven by a desire to either manipulate the critical temperature of the mixture, or to introduce polar or nonpolar features to regulate interactions of the fluid with a specific compound; ref. Supercritical Fluid Engineering Science, Erdogan Kiran, Joan F. Brennecke, ed., ACS Symposium Series 514, American Chemical Society, Washington, DC 1993, pp. 2, incorporated herein by reference.

Notwithstanding all of the above, the problem of how to construct and operate an automated supercritical fluid cleaning process for satisfactory effect on semiconductor wafers and other precision surfaces remains unresolved in the prior art.

Summary of Invention

The invention, simply stated, is a process for cleaning precision surfaces such as the cleaning of photoresist off semiconductor wafers as part of the semiconductor fabrication process. The process relies on the use of process materials such as carbon dioxide that tend to be good solvents especially at supercritical temperature and pressure, alone or in combination with useful additives such as cosolvents and surfactants selected to shift the critical point downward or improve the cleaning effect. The process materials are applied to the substrate preferably exclusively in gaseous and supercritical states so as to avoid the problems associated with liquid contact.

Soak and agitation steps are applied to the substrate to aid both chemically and mechanically in the removal of the unwanted material from the substrate. The soak step permits infusion of the process materials into the unwanted matter at an elevated supercritical pressure. The agitation step includes a rapid decompression of the process chamber after the soak period, still within supercritical pressure, in order to mechanically weaken and break loose pieces of the photoresist, sidewall polymer and such other materials as are sought to be removed, with a very significant pressure differential. This is combined with a supercritical fluid flush to carry away the loose debris, and is then preferably concluded by rapidly elevating the vessel pressure back to the higher supercritical pressure, stressing the unwanted material this time with rapid compression. The core process steps are preceded and followed by more conventional loading and unloading steps, except that the purging and pressurization steps avoid any liquid contact with the substrate, constraining the inflowing process materials to process gas and supercritical fluid.

It is therefore an objective of the invention to provide a dry process for cleaning of precision surfaces using supercritical fluids such as carbon dioxide, alone or in combination with suitable additives such as cosolvents and surfactants. It is a further object to agitate a substrate after suitable exposure to a supercritical fluid or mixture

under a higher supercritical pressure, with a rapid decompression of a significant degree.

It is a yet further object to combine a rapid decompression step with a full flow supercritical fluid or mixture flush or wash of the substrate, in order to further loosen and evaluate any loose debris, and to further expose the unwanted materials on the substrate to the solvent effects of the process materials. It is another object to illustrate the salient points of an apparatus by which the process may be conducted.

What follows is a preferred embodiment process only, and should not be interpreted as limiting of the invention.

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Brief Description of the Figures:

Fig. 1 is a rear elevation of a pressure vessel apparatus with which to carry out the process of the invention, illustrated with the pressure vessel cover in the up and closed position.

Fig. 2 is a rear elevation of the apparatus of Fig. 1, with the pressure vessel cover in the down and open position, exposing the wafer.

Fig. 3 is a top plan view of the pressure vessel apparatus of Fig. 1, the dotted line circles representing the pressure chamber and wafer in process.

Fig. 4 is a horizontal cross section view of the apparatus of Fig. 1, revealing the process chamber with divergent and convergent fluid flow channels.

Fig. 5 is a diagrammatic partial cross section elevation view through the pressure chamber of the apparatus of Fig. 1, illustrating the upper and lower heating and cooling platens, and the fluid flow through the chamber.

Fig. 6 is a simplified schematic of the process fluid supply and recovery system supporting the pressure vessel apparatus of Fig. 1, also relating to Figs. 9 and 10.

Fig. 7 is a flow chart of the process steps of the invention, illustrating the preferred and alternative preferred embodiments of the process sequence.

Fig. 8 is a phase diagram illustrating the temperature/pressure relationship to the phase or state and the critical pressure/temperature point of the preferred embodiment process fluid, carbon dioxide.

Fig. 9 is a time line chart of pressure and flow in the pressure vessel of the apparatus of Fig. 1, also relating to Figs. 6 and 10, during a sequence of twice repeated soak and

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agitate steps of the invention process, illustrating the rapid decompression and full flow parameters to which the wafer under process is subjected.

Fig. 10 is a simplified schematic of the principle apparatus components of the process fluid supply system affecting the process parameters within the process chamber, as
5 related to Figs. 6 and 9.

Description of the Preferred Embodiment:

A novel process is described for supercritical fluid cleaning of precision surfaces of substrates with or without surface features of organic material such as polymers, which includes layers of this material and related residues from various coating and/or reducing operations conducted upon the surface or its features, and inorganic material, which includes foreign particle matter. In the preferred embodiment that follows, a method for conducting the supercritical fluid stripping of photoresist and the removal of residues from related processing steps from semiconductor wafers will be described. It will be understood by those who are skilled in the art that the cleaning method is not limited to semiconductor wafers but can be applied to other substrates too.

The supercritical fluid cleaning method can be applied at various levels of the semiconductor chip manufacturing, from front end to back end with no limitation to materials or size of the wafer, where the wafer with the photoresist on it undergoes various treatments, such as ion implantation, etching, and other methods that modify the material in the layer below the photoresist, and the photoresist itself.

In the preferred embodiment described below, carbon dioxide, CO_2 , is the preferred process chemical, but the cleaning method is not limited to CO_2 . CO_2 has been selected because of low values for T_c (31.1°C) and p_c (1070.4 psi), which represents the most economical set-up in terms of equipment and operating cost, safety and health aspects and environmental issues. The supercritical state of CO_2 will be called SCCO_2 .

The properties of the process substance can be modified by additives, which can be either organic solvents, surfactants, other chemicals like chelating agents or mixtures thereof. Throughout the following description a solvent added to the CO_2 is called a "cosolvent", which can consist of more than one chemical to form a binary or a ternary, and so forth, mixture with the CO_2 . If not otherwise specified, the term "process chemical" denotes CO_2 or CO_2 + additive as a generic term. Generally an additive is

required to reduce the operating pressure of the process chemical in its supercritical state to a minimum. The additive supports the cleaning process by introducing the component of chemical interaction. Additives other than solvents, such as surfactants, can likewise be included in the process described.

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Referring again to the manufacturing of semiconductor chips, single wafer processing as opposed to batch processing is the method of choice because of the ever-increasing commercial value of the wafer with size and number of manufacturing steps, and because of quality control requirements. Therefore, in the preferred embodiment of the process equipment, a single wafer is being processed. If tolerated by the nature of the substrate and the specific cleaning requirements, the process equipment can be modified to hold multiple substrates or cassettes of substrates of various sizes, or other suitable equipment utilized.

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Referring to Figs. 1, 2, 3 and 4 showing an apparatus by which the preferred embodiment may be practiced, process chamber 10 consists of a cylindrical cavity with inlet and outlet manifold 12, 14, and lid 30. The process chamber 10 is designed such that an automatic wafer handling system typical to the semiconductor industry can be used to load the wafer into the chamber, but any other wafer loading system including manual loading can be applied too. A master control system for the apparatus shown and the associated fluid supply and recovery system is assumed. In most cases, pressure vessel process control will be further integrated into the control system of the wafer processing system with which the pressure vessel is associated.

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The process chamber 10 is located above the wafer plane in the open cover position (Fig. 2). The process chamber does not move nor does it have any moving parts. To close the process chamber, the lid 30 carrying an elastomeric type of seal 37 is moved up linearly towards the seal seat. Upon locking, the seal undergoes compression by axial forces only, from beneath the lid. This minimizes greatly the generation of particulates in the proximity of the pressure chamber. Furthermore, the seal of the lid is located below the wafer plane further eliminating the risk of adding particulates to the wafer upon

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closing and locking. The locking mechanism is sealed from the process chamber by a bellows 38. There are no moving parts of the apparatus exposed below, in or above the plane of the wafer other than the lid and bellows, during the opening, closing and locking procedures. Suitable locking mechanisms are described in the priority documents cited
5 above.

Referring to Fig. 4, the process chemical enters the process chamber 10 through a first manifold block 12 and is directed through a divergent flow path 22 into the chamber cavity 20. On the opposite side of the chamber a convergent flow path 24 directs the CO₂ out and into a second manifold block 14. The geometries of the flow paths and process chamber provide a well distributed flow pattern through the chamber insuring that the full surface area of the wafer is exposed to flow. For a design maximum flow rate of 8 lb/min of process chemical for the preferred embodiment apparatus, the internal height and volume of the chamber cavity has been chosen to prevent the flow from choking.
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Referring again to Fig. 4, the manifold blocks 12 and 14 serve multiple functions. CO₂ supply lines for process chamber inlet 11 and outlet 13 are connected with the manifold blocks. In addition, one block holds a thermocouple 26 to measure the temperature in the chamber close to the wafer. The other one has a window 15 to
15 optically monitor the wafer during the process. The symmetry of the internal chamber design permits fluid flow in either direction, with suitable line switching capability, so that the process effects can be applied singularly or alternately from either direction across the wafer under process.
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The chamber can be closed off with shut-off valves 52, 54 (Fig. 6) at inlet 13 and outlet 11 (Fig. 3). A soak step will be realized this way. Inlet and outlet valves can be individually opened or closed by the master control system.
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Referring to Fig. 2 and 5, the process chamber 10 is equipped with heater platens 32 and 33 that provide for controlling the temperature in the process chamber. The outer diameter of the platens is slightly smaller than the inner diameter of the process chamber
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so that the platens can be replaced if needed. The lower platen 32 is mounted to the chamber lid 30. Wafer mounting studs 34 are mounted on platen 32. The upper platen 33 is mounted to the ceiling of the chamber cavity 20. The platens can be heated and cooled simultaneously or set to different temperatures. The wafer is located between the platens, preferably in the middle between the platens (Fig. 5) when the chamber is closed.

In the preferred embodiment the maximum pressure cavity temperature is 150°C. Therefore the wafer will never be heated to a temperature above 150°C, which is beneficial for semiconductor wafer manufacturing in so far as this process does not add to the thermal budget of the wafer. Changing the temperature of the platens is achieved by changing the temperature of the heating/cooling medium (Fig. 5). In one embodiment, the heating/cooling loop consists of a heater set to a desired high temperature ($< 150^{\circ}\text{C}$) and a chiller set to a desired low temperature ($> 25^{\circ}\text{C}$). Applying heating/cooling medium from the respective reservoir simply changes the temperature in the process cavity from hot to cold or vice versa quickly. With this method, a temperature change of the platens 32 and 33, of from 25°C to 150°C can be performed in about one (1) minute. Using the platens to control the process temperature in the chamber rather than heating the whole chamber mass provides a means of quickly changing phases of the process chemical during the process. Therefore, the described heating/cooling platens enable better control of an additional process variable, the process temperature T , in addition to the pressure p . Varying the process temperature of both platens simultaneously allows switching between supercritical and liquid states while holding the pressure $p > p_c$. Setting the platens to different temperatures can be done to generate convective currents in the process fluid.

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Referring to Fig. 5, the wafer is normally loaded and rests face up horizontally on three studs 34 mounted to the lower platen 32. Subject to configuring the transport and loading mechanism appropriately, the wafer can be loaded and processed face down, providing a gravitational component to the cleaning process for preventing loose particulate matter from contacting or re-depositing on the critical surface.

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The studs, separated by 120° (see also Fig. 4), feature edge restraints such that the wafer cannot skid off of them in the horizontal plane by the drag of the process chemical while it flows through the process chamber. In order to prevent vertical lifting of the wafer the studs have counter parts 36 mounted to the upper platen 33 at exact the same positions as the lower studs. When the chamber is closed upper and lower studs build a vertically oriented rod with a slit to hold the wafer. The midlevel holding arrangement of studs 34 and 36 provide effective cleaning of both sides of the wafer.

As described above, pressure p [psi] and temperature T [$^\circ\text{C}$] are process parameters and are most usefully measured in the chamber of this apparatus. Other process parameters are flow rate \dot{m} [lb/min] or \dot{V} [cm^3/min], amount of additive n [mol%] or [cm^3/min], and time t [sec]. The process as described below is performed between two sets of parameters, with the index "0" denoting high values, for example $p_0 = 3,500$ psi and $T_0 = 150^\circ\text{C}$ for the preferred embodiment, and the index "1" denoting low values, for example $p_1 = 1500$ psi and $T_1 = 100^\circ\text{C}$. The temperature and the lower pressure are selected such that the process chemical is kept at supercritical state at all times. The higher pressure is selected to provide a higher solubility of polymer components in CO_2 and a maximum pressure differential during decompression, within the safe limits of the mechanical system. The pressure ratio being preferably at least 2:1.

Referring to Figs. 6 and 10, the process chemical can be supplied by the supply system in 6 variations: (i) gaseous CO_2 , (ii) supercritical CO_2 , (iii) supercritical CO_2 + cosolvent, (iv) supercritical CO_2 + surfactant, (v) liquid CO_2 , (vi) liquid CO_2 + surfactant. Referring to Fig. 6, the supply system 50 includes a storage tank 56, which is part of the CO_2 delivery system 50, containing high purity CO_2 , a flow meter 58, a liquid CO_2 pump 60, three supercritical lines 62, 72, 82, two gas lines 94 and 92, and one liquid line 102. All lines merge into one single line, which is the inlet 13 of the process chamber 10.

The pressure in the system and specifically in the process chamber is built up by a backpressure regulator 124 that is part of the outlet line of the process chamber. The process chemical expands behind the backpressure regulator into a separator tank 126

such that the CO₂ evaporates and the additive is collected. The separator is designed to avoid dry ice formation and plugging of lines. Inlet and outlet lines of the process chamber are equipped with shut-off valves 52 and 54, located close to the process chamber. In order to deliver a constant flow of CO₂ it is desired that the CO₂ supply in the storage tank 56 be kept at constant pressure. The preferred pressure is 800 psi and is maintained by control of temperature. The desired temperature is close to 20°C at which the CO₂ has a vapor pressure of 800 psi. Any other temperature and pressure setting below the critical point can be chosen.

In order to maintain the integrity of the phases of the process chemical, inlet and outlet lines of the process chamber 10, and valves 52, 54 are heated to the desired process temperature as indicated by the dotted lines in Fig. 6.

The CO₂ delivery system 50 allows charging the process chamber 10 with either the process chemical in the gas, the liquid or the supercritical state. Pressurizing the process chamber with supercritical process chemical is desired for some processes such as dry resist develop. Using supercritical process chemical instead of liquid one prevents pattern collapse of high aspect ratio structures, as noted in Environmental News, Vol. 35, Issue 7, pp. 140A - 141A, which is incorporated herein by reference.

Referring to Fig. 7, the preferred embodiment cleaning method consists of 6 basic process steps:

1. Load, purge, pressurize chamber
2. Fill chamber with process chemical;
3. Soak with process chemical;
4. Provide agitation;
5. Rinse;
6. Dry, vent, unload chamber

Process steps 1 and 6 are necessary pre and post process steps to the core steps of the process; fill, soak, agitate, and rinse. These principle process steps 2 through 5, or alternatively, steps 3 and 4 or step 4, within the sequence of steps 2 to 5, can be repeated as many times as needed in a process cycle to satisfy the user's requirement. It will be readily apparent to those skilled in the art that the soak and agitation steps are fundamental to the cleaning process of the invention, and that repetition of these two steps or of other combinations of the basis process steps will provide additional cleaning effect to the wafer under process. In other variations on the process cycle, steps 3 and/or 5 may be skipped in one or more iterations of the sequence of a full process cycle.

Process parameters can be modified between or during a process cycle, and the process chemicals can be varied if required, as well. In its entirety, the 6 process steps of the invention describe a "one step" dry-to-dry process that combines photoresist stripping, residue removal, and drying.

The basic process steps are described in detail, in the context of the enabling apparatus illustrated in the figures, as follows:

1. Load, purge, and pressurize

Once the wafer is positioned on studs 34 as described above, lid 30 moves in a linear motion towards the process chamber 10. While the lid is moving, gaseous CO₂ flows through a dedicated line 92 into the process chamber with the outlet valve 54 closed. When lid 30 (Fig. 2) approaches its final position 30 (Fig. 1), the gap between the seal and the seal seat is getting smaller. Gaseous CO₂ is now leaving the process chamber through this gap generating a forced flow of CO₂ gas from the inside towards the outside of the chamber through the gap. The flow of CO₂ gas into the process chamber is adjustable but kept constant by means of a mass flow controller 91. Therefore, with the decreasing gap between seal and seal seat, the CO₂ flow through the gap from the inside of the process chamber to the outside is increasing in velocity. The outflow velocity reaches its maximum in the moment just before the lid is locked to close the chamber, i.e. when the gap is reduced to a minimum. This gaseous CO₂ flow carries any particulates

that may be generated when the seal touches its seat away from the wafer and the chamber. The wafer is thus prevented from being contaminated by particulates of this source.

5 Once the chamber is closed and locked, the CO₂ continues to flow, which results in an increase in pressure in the process chamber. The gaseous CO₂ pressure is a variable but typically limited to 28 psi by a pressure regulator 90. The outlet valve 54 of the chamber as well as valve 128 and backpressure regulator 124 will be opened and the chamber will be purged with a continuous flow of gaseous CO₂ to replace the air that is
10 trapped in it. The process control parameter is the purge time. Pressure and flow rates of gaseous CO₂ are preset.

 Prior to pressurization of the chamber, the gas supply system is conditioned such that all supply lines 62, 72, 82 are filled with CO₂ and are set to a pressure of 800 psi up
15 to the inlet valve of the process chamber. The temperature of the system, which includes the heater platens 32 and 33 in the process chamber, will be set to the desired operating temperature T_0 with $T_0 > T_c$, and the outlet valve 54 of the process chamber is closed. The process chamber is then charged with gaseous CO₂ through another dedicated line 94 out
20 of the CO₂ storage tank 56 and pressurized to a pressure of 800 psi, which is the equilibrium pressure of the CO₂ vapor in the storage tank.

 Although one line for gaseous CO₂ would be sufficient to supply gaseous CO₂ to the process chamber, the preferred embodiment apparatus provides two lines, one, 92, for
25 purge, and another, 94, for pressurization. The second gaseous CO₂ line is directly connected with the CO₂ storage tank and has a valve arrangement for shut-off, 96, and
30 variable flow, 95. With increasing pressure in the process chamber, the flow through this line is being increased continuously to minimize the time to pressurize till finally the line connecting the storage tank and the process chamber is completely open with the pressure in the process chamber being at 800 psi or at the same pressure as the CO₂ vapor in the storage tank 56. The gaseous supply line is then closed.

In the preferred pressurization procedure, the pressure chamber 10 is being pressurized with CO₂ in gas and supercritical phase, avoiding the liquid phase. To achieve this, lines 62, 72, and 102 are closed. Line 82 and inlet valve 52 will be opened once the pressures on both sides of the inlet valve 52 are equal and at 800 psi. Inlet valve 54 is then opened and the CO₂ pump 60 delivers liquid CO₂ into line 82. At the initial pressure of 800 psi the CO₂ is transferred into its gas state on its way through the heater 51 as indicated by the arrow in Fig. 8. Upon material transport into the pressure chamber its pressure will be increasing. Since the temperature in the heated supply line and in the process chamber is at $T_0 > T_c$, the CO₂ in the process chamber initially remains a gas. Once the pressure has increased to a pressure $p > p_c$ the CO₂ in the chamber is transferred into its supercritical state. The pressurization sequence ends once pressure p_0 is reached. The process chamber is now charged with supercritical CO₂ with the CO₂ in its supercritical state. The time budget for this step of the preferred embodiment method is 70 seconds, although longer or shorter times may be appropriate, depending on the wafers to be cleaned, the selected process fluids and parameters, and various equipment limitations.

2. Fill chamber with process chemical

During the pressurization procedure the backpressure valve 124 is preset to the desired operating pressure p_0 . Once the pressure in the pressure chamber has reached p_0 , the outlet valve 54 is opened and the supercritical CO₂ flows continuously through the pressure chamber at the desired operating pressure p_0 , temperature T_0 , and constant flow \dot{m}_0 monitored by the flow meter 58. To prepare for the fill step, line 82 is closed and line 62 is opened simultaneously with the CO₂ now flowing through the cosolvent line. Referring to fig. 10, flow of process chemical is maintained constant by a PID loop connecting flow meter 58 and pump 60. The pressure is controlled by a PID loop comprising back pressure regulator and pressure transducer reading the pressure in the process chamber.

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With the CO₂ flow \dot{m}_0 known, the cosolvent metering pump 61 is set to deliver an amount n in cm³/min of cosolvent into the flow of CO₂ to achieve a concentration of preferably 2 to 8 vol%. The mixture of CO₂ and cosolvent, called the process chemical, is transformed into its supercritical state while passing through heater 51. It enters the process chamber through heated lines, which maintain the supercritical state during flow. The critical point of the binary process chemical shifts towards higher values as compared to pure CO₂. The concentration of the cosolvent in CO₂ is chosen such that at $p_1 = 1500$ psi and $T_1 = 100^\circ\text{C}$ in the process chamber 10, the cosolvent does not precipitate out of solution. At a flow rate of 3 liters/min of liquid CO₂ the supercritical CO₂ of the process chamber from the previous pressurization step can be replaced in less than 10 seconds, however the preferred embodiment method budgets 40 seconds for this step.

3. Soak

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Referring to Figs. 6 and 9, there is shown a chart for process and flow as a function of time for repetitive soak and agitation steps 3 and 4. These steps can be run once in a process cycle, or with any number of repetitions, in accordance with the user's requirement. Once the chamber is filled with process chemical during the preceding Fill step, inlet valve 52 and outlet valve 54 are closed at soak start time t_0 . The process chemical in the process chamber remains at the temperature T_0 and pressure p_0 . Sometime during the soak step backpressure regulator 124 is reset to full open. During the soak period, the infusion of CO₂ and cosolvent at high pressure into the photoresist and sidewall polymer material causes swelling. It is assumed that during this swelling process mechanical stress occurs at the interface of the photoresist and polymer material to the substrate, tending to stress, weaken, and rupture the interface bond at a microscopic level. As explained above, sidewall polymers typically are fluorinated compounds that dissolve in CO₂. The cosolvent aids during the soak step to weaken and break chemical bonds within the polymer layers of the bulk photoresist reducing its average molecular weight. The soak step is static with no flow. The time budget for the soak step for the preferred

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embodiment process is 30 seconds, although longer or shorter times may be desirable depending on all other variables as described above.

4. Agitation

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Referring to Figs. 6, 9, and 10, by completion of the soak step at t_1 , outlet valve 54 is opened to apply rapid decompression to the chamber; backpressure regulator 124 having been previously set to full open so as to make the decompression as rapid as the conductance of valve 54 and the lines permit. By application of the rapid decompression step at t_1 , the photoresist and sidewall polymer material, having been previously infused with CO_2 and cosolvent under the higher pressure p_0 during the soak step, is now subjected to a dramatic stress of internal to external pressure differential, inducing a mechanical rendering, breaking up and loosening of the structure of the photoresist and the sidewall polymer as the CO_2 and cosolvent is evacuated.

15

Experiments have been carried out to investigate the absorption of CO_2 in polymeric material and its behavior upon decompression. It has been found that when rapidly decompressed significant structural changes of the polymeric material can be induced; ref. Evaluation of Supercritical Fluid Interactions with Polymeric Materials, Samuel P. Sawan, et al., in "Supercritical Fluid Cleaning - Fundamentals, Technology and Applications", John McHardy, Samuel P. Sawan, ed., Noyes Publications, Westwood, NJ, USA, 1998, pp. 130, incorporated herein by reference. In the preferred embodiment process here, the pressure vessel is maintained at the lower pressure p_1 for a sufficient period of time to dissipate the pressure differential affecting the photoresist and the sidewall material.

25

Initializing the rapid decompression is accompanied by an initial surge of outflow of process fluid. At time t_2 shortly thereafter, inlet valve 52 is opened to introduce an inflow at p_1 that will sustain the rate of outflow, thus providing a full flow washing action through the process chamber over the wafer to lift and flush the loosened and loosening material during the decompressive rendering. The inflow mixture can be altered during

30

this decompressive flush, if desired, for the repetitive soak and agitation sub cycle that is illustrated here.

Referring to Fig. 6, during the fill stage the supply side was increased to p_0 . Since
5 during rapid decompression pressure drops to p_1 , feed line 62 has to be prepared to start
delivery at p_1 for the agitation step that follows. Therefore during soak with inlet valve 52
and outlet valve 54 closed, line 62 is bled to p_1 through the bypass line 122 and valve 123
with backpressure valve 124 set to p_1 . Once p_1 is reached, valve 123 closes and
backpressure valve 124 is set to full open. The agitation step starts at t_1 as outlet valve 54
10 is opened and the pressure in the process chamber drops quickly towards p_1 . At t_2 when
the pressure vessel has bled down to p_1 inlet valve 52 is opened and supercritical CO₂ at
flow rate \dot{m}_0 is delivered through line 62 into the process chamber to sustain the rate of
outflow. Once the pressure is dropped to p_1 , backpressure valve 124 is set to p_1 and the
flow continues through the process chamber at the lower pressure. The composition of
15 the process chemical can be altered if required at any time before or during this flow by
opening alternative feed lines 72 or 82 as desired.

If the soak and agitation steps are to be repeated, then at t_3 outlet valve 54 is
closed causing the pressure in the process chamber to rise till p_0 is reached at t_4 , the end
20 of the agitation step, at which time inlet valve 52 is shut off to terminate the flow and to
reset the clock to t_0 for the next soak step.

The time budget for the agitation step for the preferred embodiment method is 20
seconds, but again, the time is variable depending on all other variables and the user's
25 requirement.

5. Rinse

If the process cycle is to be taken to completion at this point, then at t_3 outlet
30 valve 54 is closed causing the pressure in the process chamber to rise till p_0 is reached at
 t_4 , beginning the rinse step at full pressure and full flow.

Rinsing can be performed either in the liquid or the supercritical state with pure CO₂ or CO₂ + additive, e.g. surfactant. If a rinse in the liquid state of CO₂ is to be performed, the temperature in the process chamber and inlet and outlet lines have to be dropped below T_c . Rinsing is then performed by pumping liquid CO₂ or liquid CO₂ mixture through line 102. The pressure in the pressure chamber is maintained at $p > p_c$. The preferred embodiment method time budget for this step is 30 seconds, subject to the same variables as other steps.

10 6. Dry, vent, unload

Drying is performed by venting the chamber to atmosphere pressure using backpressure valve 124 as a variable orifice to control the pressure decrease. Referring to Fig. 8 the pressure in the process chamber is forced to decrease along a vertical line with $T > T_c$ and $T = \text{const}$. This technique transforms supercritical CO₂ directly into the gas state without crossing the liquid-gas boundary. Residual stains due to liquid droplet formation are prevented.

If during the rinse step CO₂ is used in its liquid state with the pressure $p > p_c$, inlet valve 52 and inlet valve 54 are closed and the temperature in the process chamber is increased to bringing the CO₂ into the supercritical state. If during the rinse step the pressure was allowed to go below p_c the pressure is first increased to above p_c before the temperature is increased, in order to insure that during temperature increase the liquid-gas boundary is not crossed accidentally. Once the pressure chamber has been vented to atmosphere pressure, gaseous CO₂ is applied as during the opening procedure for the same reason as in the closing procedure. Unloading and reloading for the next process cycle is then initiated.

The time budget for this step of the preferred embodiment method, ending when the wafer is unloaded, is 45 seconds, but is again subject to the same variables as in other steps.

The invention is susceptible of other embodiments. For example, there is a supercritical fluid cleaning process for cleaning precision surfaces on substrates such as semiconductor wafers, consisting of the steps of:

5 (a) Selecting process materials consisting of a process gas which is convertible at a critical point of temperature and pressure to a supercritical fluid for cleaning.

(b) Selecting supercritical fluid operating parameters for the process gas including a supercritical temperature, a lower supercritical pressure, and a higher supercritical pressure, with the higher supercritical pressure being preferably at least twice the lower
10 supercritical pressure.

(c) Loading, closing and sealing at least one substrate with a precision surface in a pressure vessel, where the vessel is connected to a source of process gas and a source of supercritical fluid and has at least one port for exhausting byproducts of said process. The vessel is also configured with heat exchanger platens or the like for heating the
15 interior of the vessel. And the vessel has independent means such as inlet and outlet valves for isolating the vessel from inflow of the process materials and outflow of the process byproducts.

(d) Purging and pressurizing the vessel with process gas and supercritical fluid to the higher supercritical pressure while heating the interior to the supercritical temperature
20 so as to displace all other gases with supercritical fluid without entering a liquid phase condition.

(e) Soaking the substrate at the higher supercritical pressure for a predetermined soak period, so as to infuse the materials to be removed with the supercritical fluid mixture under the higher supercritical pressure.

25 (f) Agitating the substrate by rapidly decompressing the vessel to the lower supercritical pressure so as to mechanically stress the material to be removed with the pressure differential, while flushing the vessel and the substrate with supercritical fluid for a predetermined period of time to wash out the loosened debris and particulate matter, and then rapidly elevating the vessel pressure back to the higher supercritical pressure to
30 further stress the remaining materials to be removed.

(g) Rinsing the substrate at the higher supercritical pressure.

(h) Drying the substrate with supercritical fluid and process gas by maintaining the vessel at supercritical temperature while decreasing vessel pressure to ambient. And then,

(i) Opening the vessel and unloading the substrate.

5

The vessel in this embodiment may also be connected to a source of supercritical fluid mixture consisting of the supercritical fluid and selected additives in solution, where the process includes a further step (d.1) of filling the vessel with the supercritical fluid mixture so as to replace the supercritical fluid, and consequently in step (f), flushing the
10 supercritical fluid mixture with either supercritical fluid, or fluid with such additives as desired, to be then followed by another iteration of agitation, soak and agitation, or by advancing to the rinse step. The core process steps of filling through agitating may be repeated one or more times in a given process cycle. The preferred process gas is carbon dioxide, but other process gases may be used.

15

In accordance with the goal of automating the process, the process is expected to be conducted in repetitive cycles with a processed substrate being unloaded and a new substrate being loaded in a shared step between consecutive cycles. Also, the vessel may be configured as an inverted vessel with an underside vertically operated lid upon which
20 the substrate is loaded for processing. Other embodiments may accommodate multiple substrates in stacks, arrayed in a common plane, or otherwise oriented to fit in the vessel and be effectively cleaned by process mechanisms.

The vessel heaters may be one or more heat exchanger platens in the vessel,
25 preferably two platens between which the substrate is secured for processing. While the substrate may be processed with the precision side up, the process may be conducted with double sided substrates or with the precision side down. The vessel may have a divergent inflow channel and a convergent outflow channel to facilitate an effective flow pattern across and around the substrate. Further, the vessel and fluid supply and recovery system
30 may be configured for reversing the direction of flow of the process materials through the

vessel, even during the process cycle if bi-directional flow action across the substrate is desired for more effective cleaning.

5 The vessel may also be connected to a source of a process gas mixture of process gas and selected additives, for which the process can incorporate additional or alternate steps to employ in the process, as by varying pressure between supercritical and gas states while holding temperature at supercritical level so as to avoid entering a liquid state condition. Likewise, the vessel may be connected to a source of process gas in liquid state, for circumstances when having a liquid contact the substrate is useful.

10

As another example of the invention, there is a supercritical fluid cleaning process for cleaning precision surfaces consisting of the steps:

(a) Selecting process materials comprising carbon dioxide as a process gas which is convertible at a critical point of temperature and pressure to a supercritical fluid for the
15 cleaning process, and additives soluble in the process gas.

(b) Selecting supercritical fluid operating parameters for the process gas including a supercritical temperature, a lower supercritical pressure, and a higher supercritical pressure, where the higher supercritical pressure is preferably at least twice the lower supercritical pressure, although a lesser differential may provide a sufficient benefit under
20 some circumstances.

(c) Loading, closing and sealing at least one substrate with a precision surface in a pressure vessel, where the vessel is connected to a source of process gas, a source of supercritical fluid, and a source of supercritical fluid mixture consisting of supercritical fluid and additives. The vessel has at least one port for exhausting byproducts of the
25 process, and is configured with upper and lower heat exchanger platens for heating the interior. It has independent means for isolating the interior from inflow of process materials and outflow of byproducts.

(d) Purging and pressurizing the vessel with process gas and supercritical fluid to the higher supercritical pressure while heating the interior to supercritical temperature so
30 as to displace all other gases with supercritical fluid without entering a liquid phase condition.

(e) Filling the vessel with the supercritical fluid mixture so as to replace the supercritical fluid.

(f) Soaking the substrate at the higher supercritical pressure for a predetermined soak period, so as to infuse the materials to be removed with the supercritical fluid mixture under the higher supercritical pressure.

(g) Agitating the substrate by rapidly decompressing the vessel to the lower supercritical pressure so as to mechanically stress the material to be removed with the pressure differential, and flushing the vessel with supercritical fluid or supercritical fluid mixture for a predetermined period of time to wash out the loosened debris and particulate matter, and then preferably rapidly elevating the vessel pressure back to the higher supercritical pressure to further stress the remaining materials to be removed.

(h) Rinsing the substrate with supercritical fluid preferably at the higher supercritical pressure, although lower supercritical pressures may be suitable under some circumstances.

(i) Drying the substrate with supercritical fluid and process gas by maintaining the vessel at supercritical temperature when decreasing vessel pressure to ambient without entering a liquid phase condition. And then,

(j) Opening the vessel and unloading the substrate. Opening and closing may incorporate a low pressure outgassing of process gas to facilitate removal of any remaining particulate matter through the lid opening.

As in the previous embodiment, various alternatives to the basic step sequence and vessel configuration may be incorporated to further enhance the cleaning effect.

It will be readily apparent to those skilled in the art that there are other and various embodiments within the scope of the invention as disclosed and illustrated in the figures, and in the claims that follow.

Claims:

We claim:

- 5 1. A supercritical fluid cleaning process for cleaning precision surfaces comprising the steps:
- (a) selecting process materials comprising a process gas which is convertible at a critical point of temperature and pressure to a supercritical fluid for said cleaning process,
- 10 (b) selecting supercritical fluid operating parameters for said process gas including a supercritical temperature, a lower supercritical pressure, and a higher supercritical pressure, said higher supercritical pressure being preferably at least twice said lower supercritical pressure,
- (c) loading, closing and sealing at least one substrate with a said precision surface
- 15 in a pressure vessel, said vessel being connected to a source of said process gas and a source of said supercritical fluid and having at least one port for exhausting byproducts of said process, said vessel configured with means for heating the interior thereof and having independent means for isolating said vessel from inflow of said process materials and outflow of said byproducts,
- 20 (d) purging and pressurizing said vessel with process gas and supercritical fluid to said higher supercritical pressure while heating said interior to said supercritical temperature so as to displace all other gases with supercritical fluid without entering a liquid phase condition,
- (e) soaking said wafer at said higher supercritical pressure for a predetermined
- 25 soak period,
- (f) agitating said substrate by rapidly decompressing said vessel to said lower supercritical pressure and flushing said vessel with said supercritical fluid for a predetermined period of time, then rapidly elevating said vessel to said higher supercritical pressure,
- 30 (g) rinsing said substrate at said higher supercritical pressure,

(h) drying said substrate with supercritical fluid and process gas by maintaining said vessel at supercritical temperature when decreasing vessel pressure to ambient, and
(i) opening said vessel and unloading said substrate.

- 5 2. A supercritical fluid cleaning process according to claim 1, said vessel being also connected to a source of supercritical fluid mixture comprising said supercritical fluid and selected additives in solution, said process further comprising additional step (d.1) filling said vessel with said supercritical fluid mixture so as to replace said supercritical fluid, and in said step (f) said flushing said vessel with said supercritical fluid comprising
10 said supercritical fluid mixture.
3. A supercritical fluid cleaning process according to claim 2, further comprising at least one repetition of steps (e) and (f) sequentially for at least two iterations during said process.
- 15 4. A supercritical fluid cleaning process according to claim 2, further comprising at least one repetition of steps (d.1) through (f).
5. A supercritical fluid cleaning process according to claim 1, said process materials
20 comprising carbon dioxide.
6. A supercritical fluid cleaning process according to claim 1, said process being conducted as repetitive cycles with a processed substrate being unloaded and a new said substrate being loaded for each consecutive cycle.
- 25 7. A supercritical fluid cleaning process according to claim 1, said vessel configured as an inverted vessel with an underside vertically operated lid upon which said substrate is mounted for said processing.
- 30 8. A supercritical fluid cleaning process according to claim 2, said means for heating the interior comprising at least one heat exchanger platen in said vessel.

9. A supercritical fluid cleaning process according to claim 8, said at least one heat exchanger platen comprising upper and lower platens between which said substrate is supported during said process.
- 5 10. A supercritical fluid cleaning process according to claim 2, said step (c) comprising loading and processing said substrate with said precision surface facing downward.
11. A supercritical fluid cleaning process according to claim 2, said vessel configured for
10 reversing the direction of flow of said process materials.
12. A supercritical fluid cleaning process according to claim 2, said vessel being also connected to a source of a process gas mixture of said process gas and selected additives.
- 15 13. A supercritical fluid cleaning process according to claim 12, said vessel being also connected to a source of process gas in liquid state.
14. A supercritical fluid cleaning process for cleaning precision surfaces comprising the steps:
- 20 (a) selecting process materials comprising carbon dioxide as a process gas which is convertible at a critical point of temperature and pressure to a supercritical fluid for said cleaning process, and additives soluble in said process gas,
- (b) selecting supercritical fluid operating parameters for said process gas including a supercritical temperature, a lower supercritical pressure, and a higher
25 supercritical pressure, said higher supercritical pressure being preferably at least twice said lower supercritical pressure,
- (c) loading, closing and sealing at least one substrate with a said precision surface in a pressure vessel, said vessel being connected to a source of said process gas and a source of said supercritical fluid and a source of supercritical fluid mixture comprising
30 said supercritical fluid and said additives, and having at least one port for exhausting byproducts of said process, said vessel configured with upper and lower heat exchanger

platens for heating the interior thereof and having independent means for isolating said vessel from inflow of said process materials and outflow of said byproducts,

5 (d) purging and pressurizing said vessel with process gas and supercritical fluid to said higher supercritical pressure while heating said interior to said supercritical temperature so as to displace all other gases with supercritical fluid without entering a liquid phase condition,

(e) filling said vessel with said supercritical fluid mixture so as to replace said supercritical fluid,

10 (f) soaking said wafer at said higher supercritical pressure for a predetermined soak period,

(g) agitating said substrate by rapidly decompressing said vessel to said lower supercritical pressure and flushing said vessel with said supercritical fluid for a predetermined period of time, then rapidly elevating said vessel to said higher supercritical pressure,

15 (h) rinsing said substrate with said supercritical fluid at said higher supercritical pressure,

(i) drying said substrate with supercritical fluid and process gas by maintaining said vessel at supercritical temperature when decreasing vessel pressure to ambient without entering a liquid phase condition,

20 (j) opening said vessel and unloading said substrate.

15. A supercritical fluid cleaning process according to claim 14, further comprising at least one repetition of steps (g) and (h) sequentially for at least two iterations thereof during said process.

25 16. A supercritical fluid cleaning process according to claim 14, further comprising at least one repetition of steps (e) through (h).

30 17. A supercritical fluid cleaning process according to claim 14, said process being conducted as repetitive cycles with a processed said substrate being unloaded and an unprocessed said substrate being loaded for each consecutive cycle.

18. A supercritical fluid cleaning process according to claim 14, said vessel configured as an inverted vessel with an underside vertically operated lid upon which said substrate is mounted for said processing.
19. A supercritical fluid cleaning process according to claim 14, said step (c) comprising
5 loading and processing said substrate with said precision surface facing downward.
20. A supercritical fluid cleaning process according to claim 14, said vessel configured for reversing the direction of flow of said process materials.
21. A supercritical fluid cleaning process according to claim 14, said vessel further comprising a divergent inflow channel and a convergent outflow channel.
- 10 22. A supercritical fluid cleaning process according to claim 14, said vessel being also connected to a source of a process gas mixture of said process case and said additives.
23. A supercritical fluid cleaning process according to claim 14, said vessel being also connected to a source of liquid carbon dioxide.
24. A supercritical fluid cleaning process for cleaning precision surfaces comprising the
15 steps:
- (a) selecting process materials comprising carbon dioxide as a process gas which is convertible at a critical point of temperature and pressure to a supercritical fluid for said cleaning process, and additives soluble in said process gas,
- (b) selecting supercritical fluid operating parameters for said process gas
20 including a supercritical temperature, a lower supercritical pressure, and a higher supercritical pressure, said higher supercritical pressure being preferably at least twice said lower supercritical pressure,
- (c) loading, closing and sealing at least one substrate with a said precision surface in a pressure vessel, said vessel being connected to a source of said process gas and a
25 source of said supercritical fluid and a source of supercritical fluid mixture comprising said supercritical fluid and said additives, and having at least one port for exhausting byproducts of said process, said vessel configured as an inverted vessel with an underside vertically operated lid upon which said substrate is mounted for said processing, said

vessel further comprising a divergent inflow channel and a convergent outflow channel, said vessel configured with upper and lower heat exchanger platens for heating the interior thereof and having independent means for isolating said vessel from inflow of said process materials and outflow of said byproducts,

5 (d) purging and pressurizing said vessel with process gas and supercritical fluid to said higher supercritical pressure while heating said interior to said supercritical temperature so as to displace all other gases with supercritical fluid without entering a liquid phase condition,

(e) filling said vessel with said supercritical fluid mixture so as to replace said
10 supercritical fluid,

(f) soaking said wafer at said higher supercritical pressure for a predetermined soak period,

(g) agitating said substrate by rapidly decompressing said vessel to said lower supercritical pressure and flushing said vessel with said supercritical fluid for a
15 predetermined period of time, then elevating said vessel to said higher supercritical pressure,

(h) rinsing said substrate with said supercritical fluid at said higher supercritical pressure,

(i) drying said substrate with supercritical fluid and process gas by maintaining
20 said vessel at supercritical temperature when decreasing vessel pressure to ambient without entering a liquid phase condition,

(j) opening said vessel and unloading said substrate.

25 25. A supercritical fluid cleaning process according to claim 14, further comprising at least one repetition of steps (g) and (h) sequentially for at least two iterations thereof during said process.

26. A supercritical fluid cleaning process according to claim 14, further comprising at least one repetition of steps (e) through (h).

27. A supercritical fluid cleaning process according to claim 14, said process being
30 conducted as repetitive cycles with a processed said substrate being unloaded and an unprocessed said substrate being loaded for each consecutive cycle.

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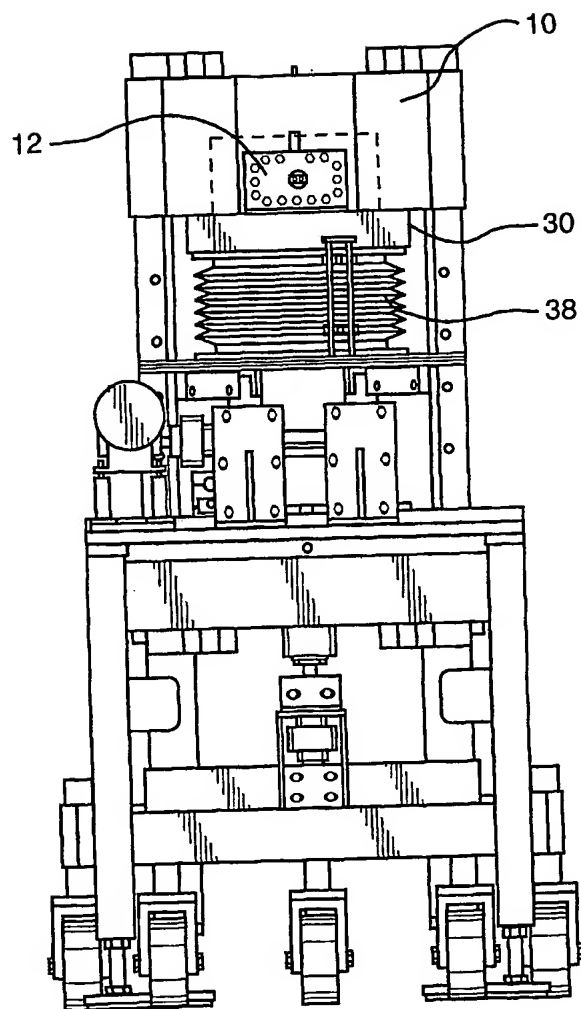


FIG. 1

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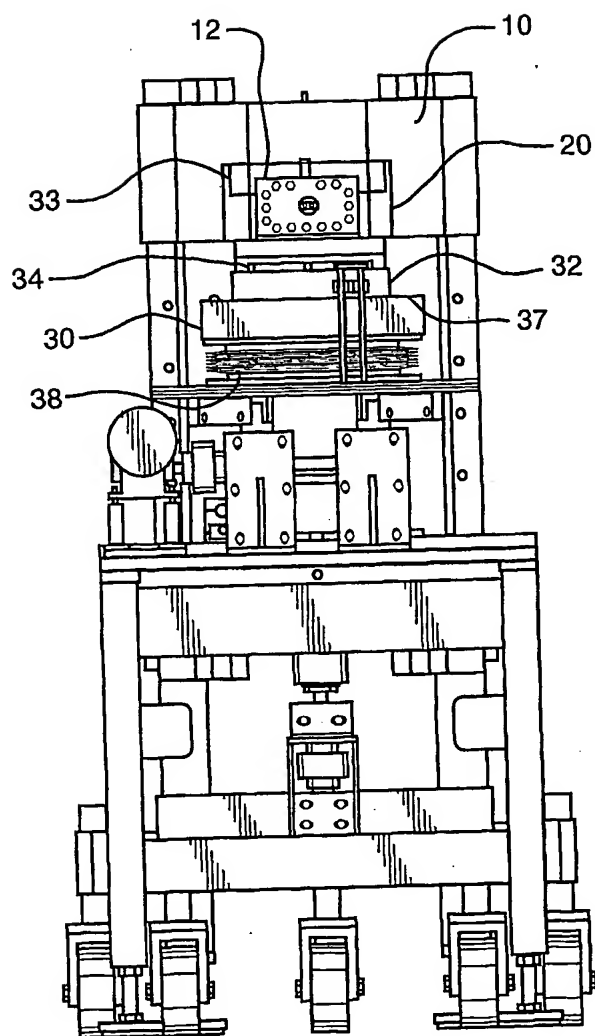


FIG. 2

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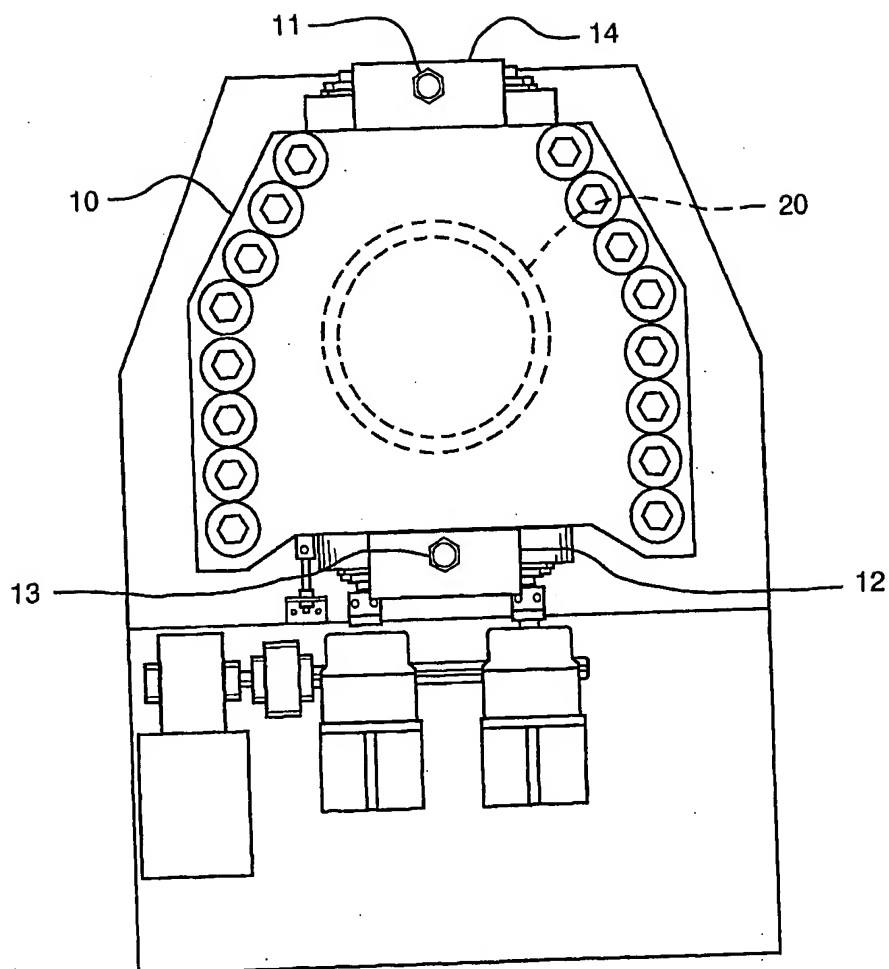


FIG. 3

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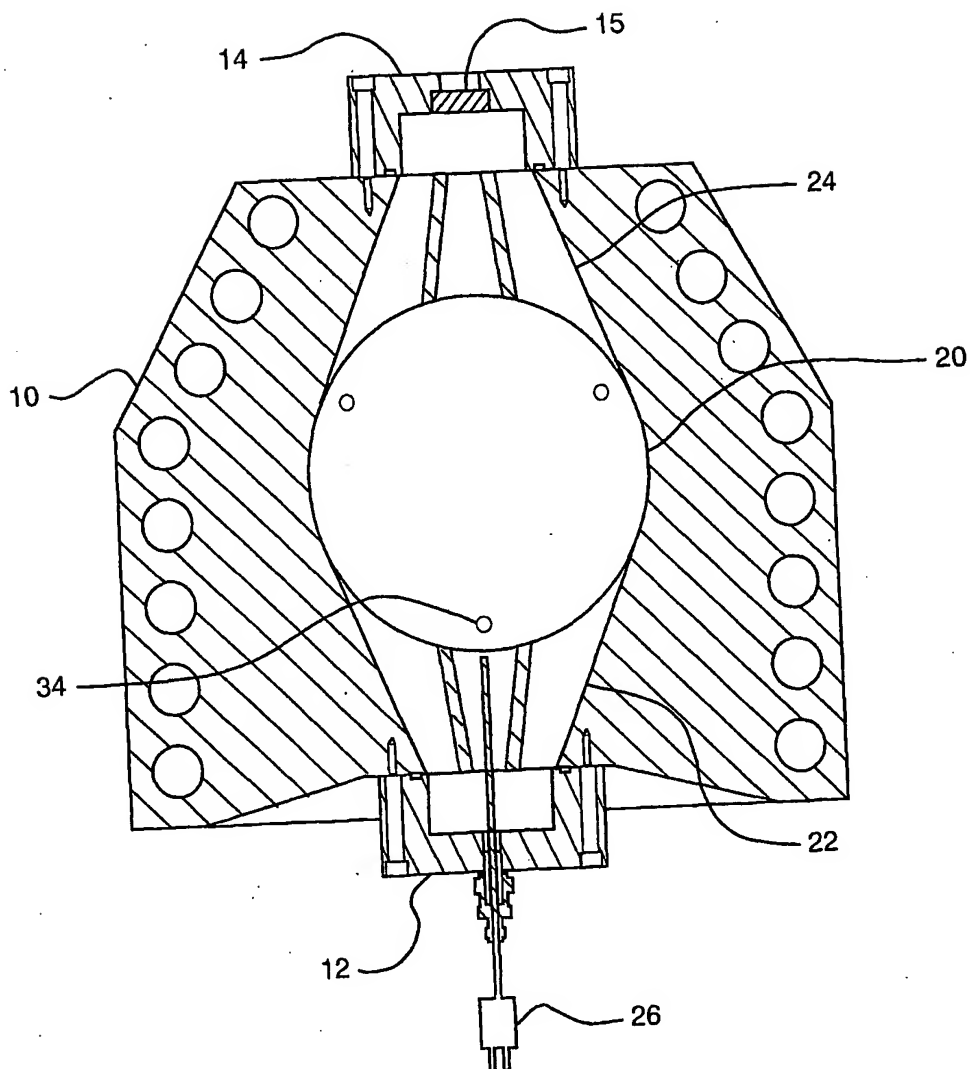


FIG. 4

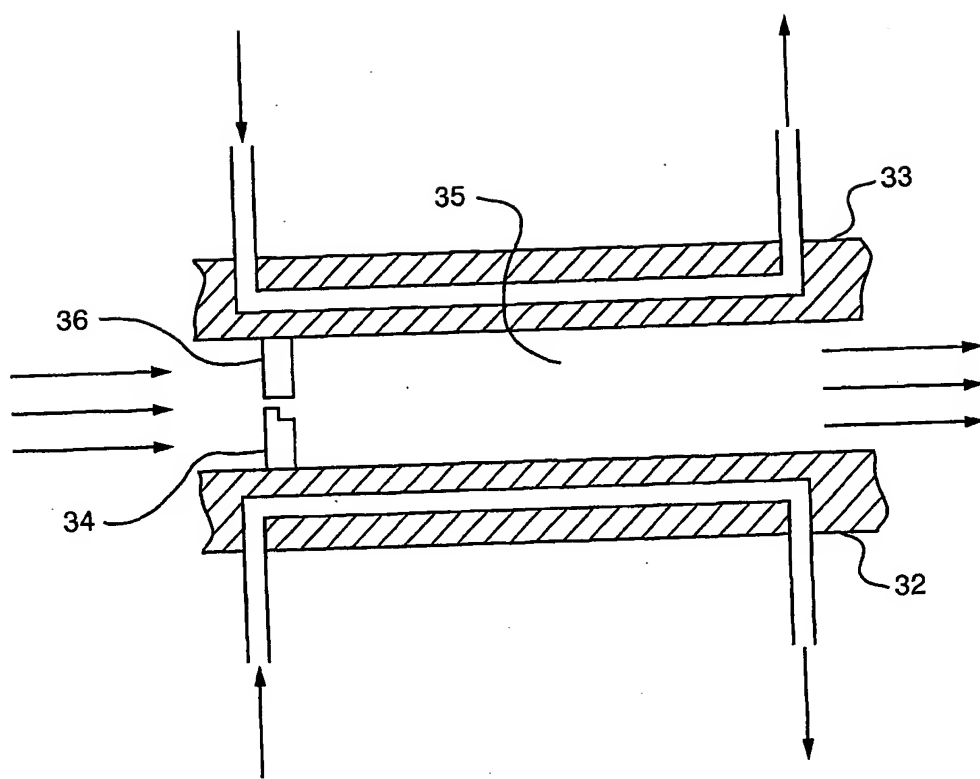


FIG. 5

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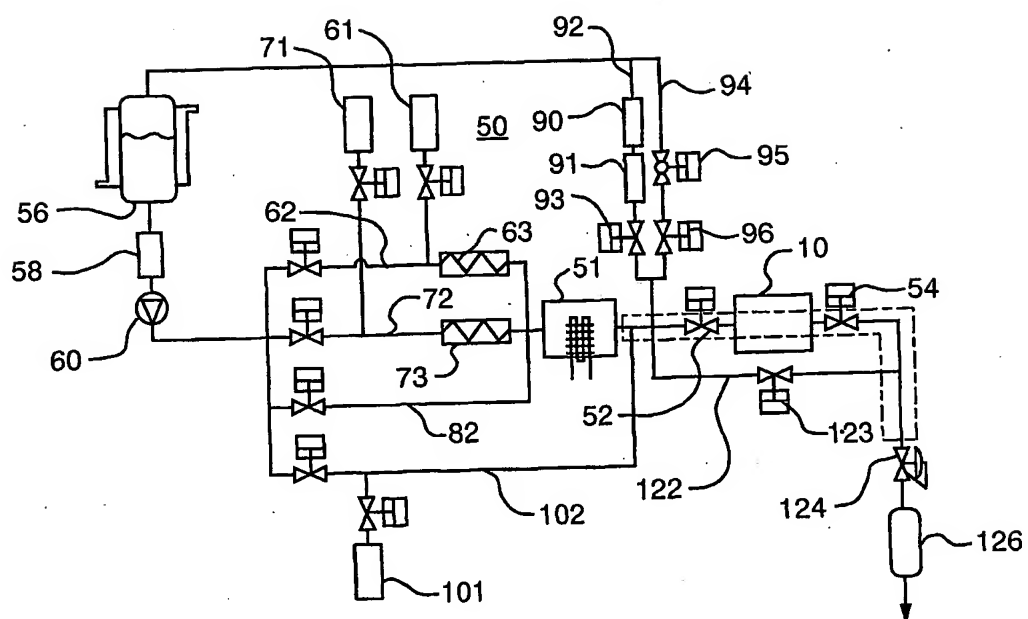
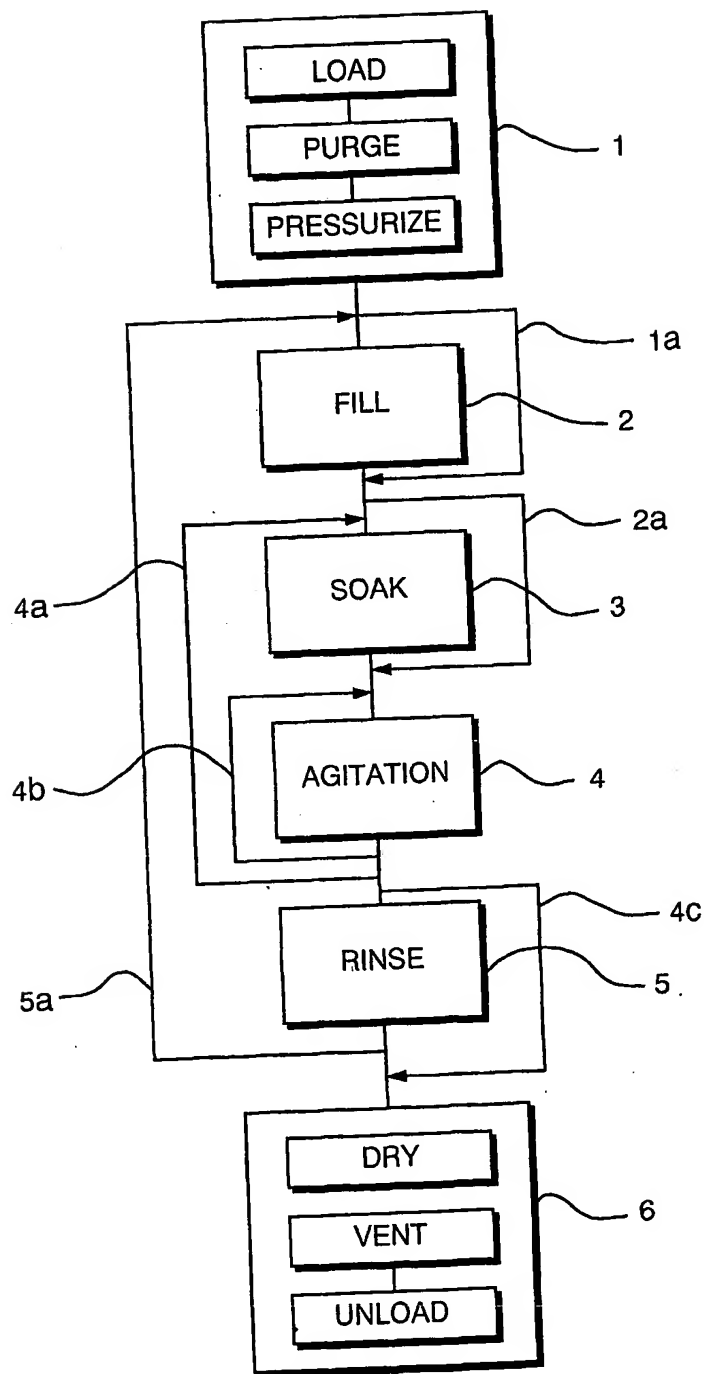


FIG. 6

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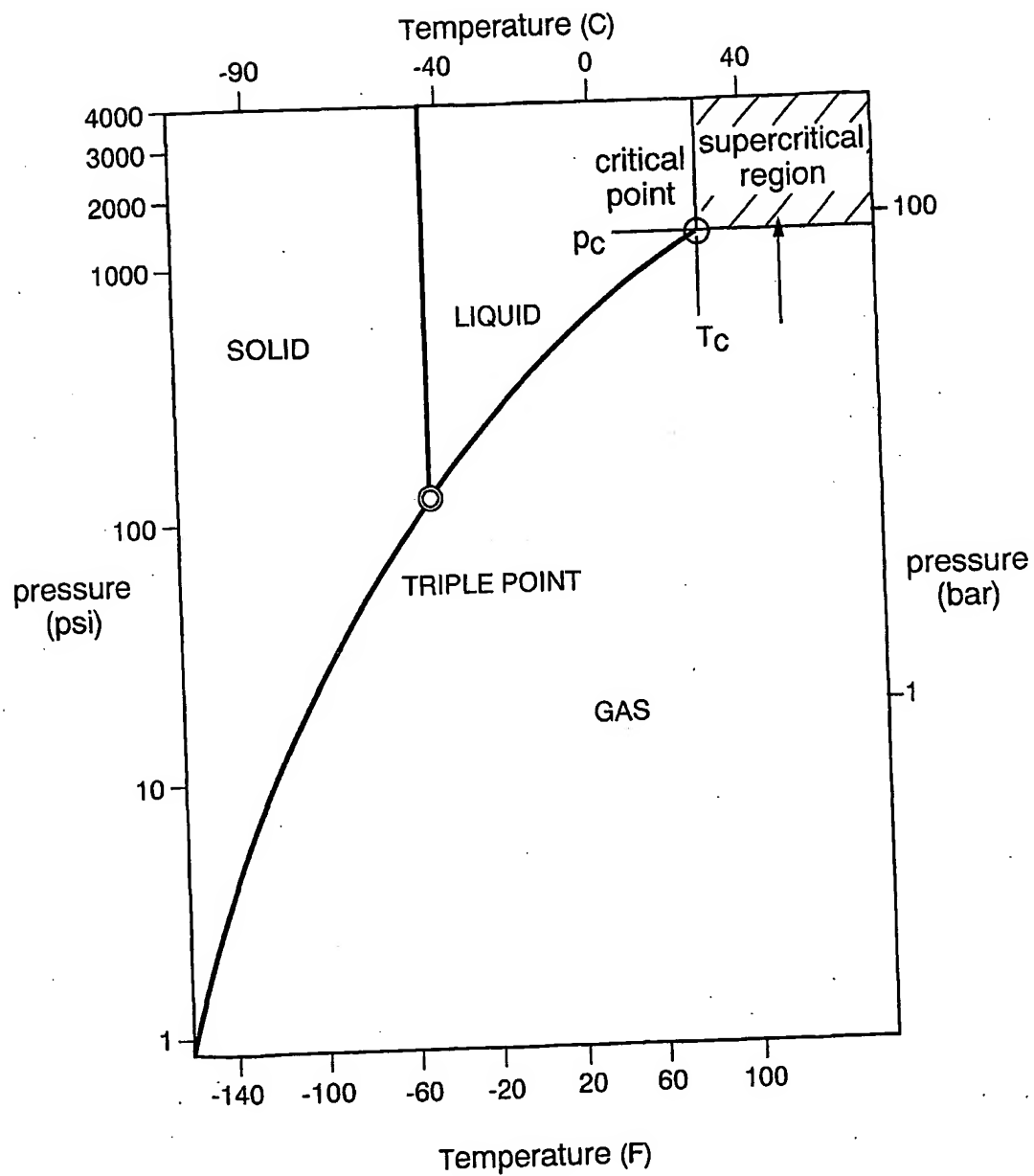


FIG. 8

SUBSTITUTE SHEET (RULE 26)

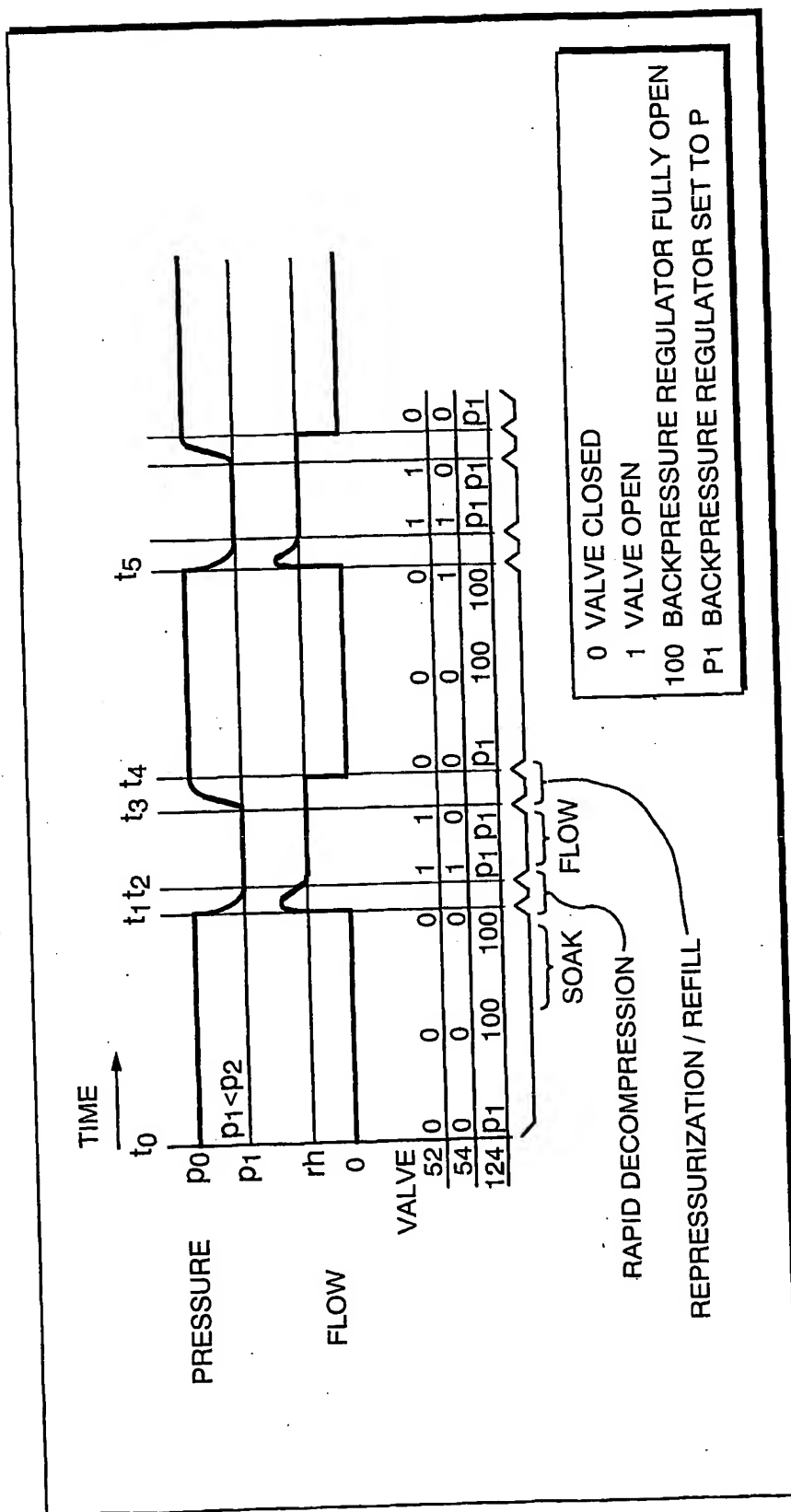


FIG. 9

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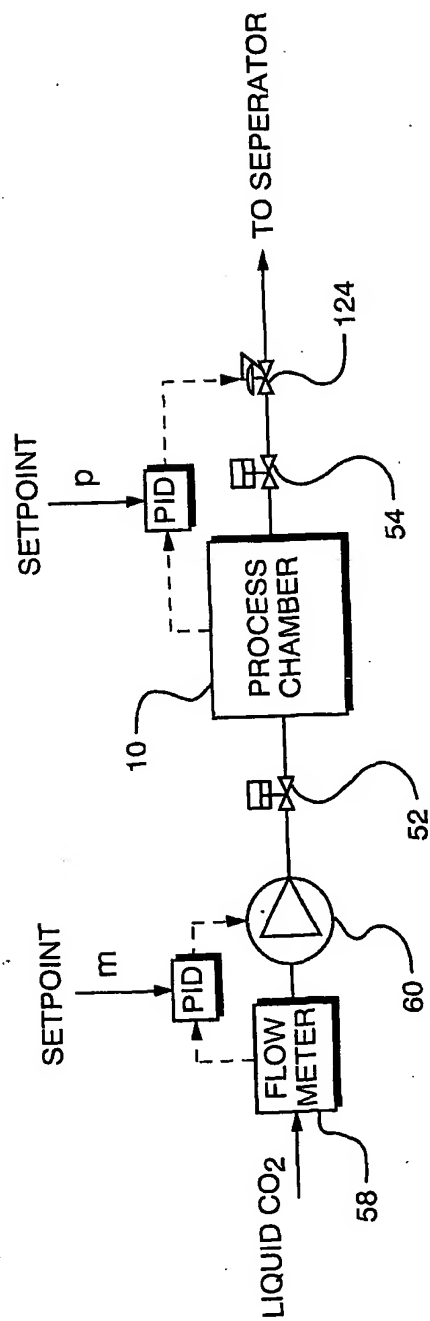


FIG. 10

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US01/15999

A. CLASSIFICATION OF SUBJECT MATTER

IPC(7) :B06B 5/00

US CL :134/37

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 134/37, 11, 17, 21, 25.4, 42, 200, 902

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched
NONE

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

NONE

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 3,968,885 A (HASSAN et al.) 13 JULY 1976 (13.07.1976).	1-27
A	US 4,355,937 A (MACK et al.) 26 OCTOBER 1982 (26.10.1982).	1-27
A	US 4,827,868 A (TAKEI et al.) 09 MAY 1989 (09.05.1989).	1-27
A	US 5,013,366 A (JACKSON et al.) 07 MAY 1991 (07.05.1991).	1-27

☒ Further documents are listed in the continuation of Box C. ☐ See patent family annex.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be of particular relevance	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"B" earlier document published on or after the international filing date	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"G" document member of the same patent family
"O" document referring to an oral disclosure, use, exhibition or other means	
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search
04 AUGUST 2001Date of mailing of the international search report
30 AUG 2001Name and mailing address of the ISA/US
Commissioner of Patents and Trademarks
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INTERNATIONAL SEARCH REPORT

International application No.
PCT/US01/15999

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 5,169,408 A (BIGGERSTAFF et al.) 08 DECEMBER 1992 (08.12.1992).	1-27
A	US 5,306,350 A (HOY et al.) 26 APRIL 1994 (26.04.1994).	1-27
A	US 5,314,574 A (TAKAHASHI) 24 MAY 1994 (24.05.1994).	1-27
A	US 5,368,171 A (JACKSON) 29 NOVEMBER 1994 (29.11.1994).	1-27
A, P	US 6,090,217 A (KITTLE) 18 JULY 2000 (18.07.2000).	1-27
A, P	US 6,092,538 A (ARAI et al.) 25 JULY 2000 (25.07.2000)	1-27